72nd BHT Colloquium

KK5: Sustainability, recycling and secondary metallurgical processes 2







June 09-11



















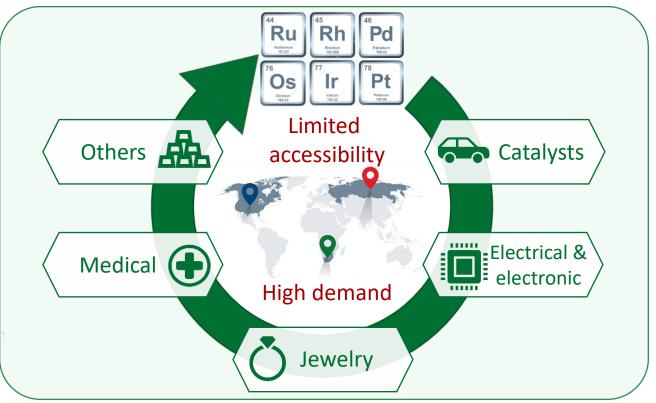






Introduction





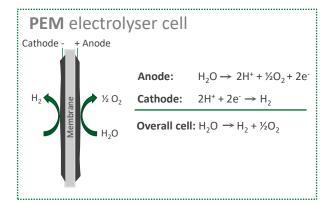




Main objective



Aim: Develop recycling approach for PGM recovery from proton exchange membrane (PEM) electrolysers



Electrode composition

Pt (PtRu alloy NPs) 22%

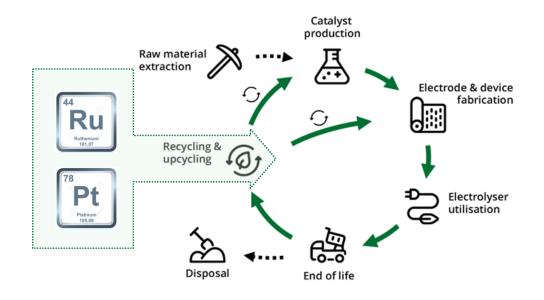
Ru (PtRu alloy NPs) 11%

Carbon NPs 11%

Carbon substrate 41%

■ NafionTM 15%







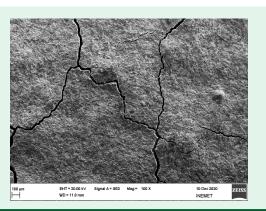


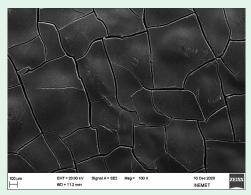
Pre-treatment procedure

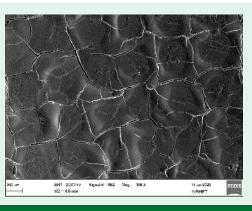


Treatment of PtRu-based electrode with the alkyl alcohol

Catalyst layer
PtRu alloy
C NPs
NafionTM



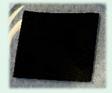




SEM images (× 100): PtRu-based electrode material

C-substrate (new)

C-substrate after treatment



Electrode (100%)

- Ethanol
- Isopropanol
- Ultrasound





Dissolved catalyst layer





(59%)

Dry residue





This Project has received funding from the European Union's Horizon 2020 Research and Innovation Programme under Grant Agreement N. 861960





Hydrometallurgical approach

HCI + HNO₃ 88% Ru; 97% Pt

HCl + H₂O₂91% Ru; 100% Pt

$$NO_3^- + 4H^+ + 3e^- \rightarrow NO + 2H_2O \quad E^0 = 0.96V$$

$$H_2O_2 + 2H^+ + 2e^- \rightarrow 2H_2O$$
 $E^0 = 1.77V$

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Leaching efficiency:

$$\frac{c(PGM\ in\ sol.)*V(sol.)}{m(sample)*w(PGM\ content)}*100\%$$

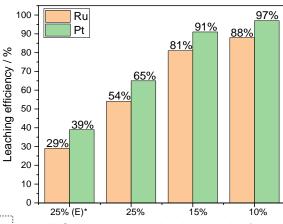




$$Pt^{4+} + 4e^{-} \rightarrow Pt$$
 $E^{0} = 1.15V$
 $[PtCl_{6}]^{2-} + 4e^{-} \rightarrow Pt + 6Cl^{-}$ $E^{0} = 0.74V$
 $[RuCl_{6}]^{2-} + e^{-} \rightarrow [RuCl_{6}]^{3-}$ $E^{0} = 0.83V$

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Leaching conditions: 12M HCl, 75 °C, 3h



HNO₃ concentration in leaching solution / vol% *E - Electrode





HCl-based leaching system

H₂O₂ content (1-5%, 7.5%, 10%, 20%)

HCl concentration (2M, 3M, 4M, 8M, 12M)

Additives (NaCl, CuCl₂, AlCl₃)







+ RECYCALYSE -

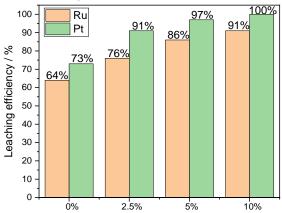
HCI-based leaching system

H₂O₂ content (1-5%, 7.5%, **10%**, 20%)

HCl concentration (2M, 3M, 4M, 8M, 12M)

Additives (NaCl, CuCl₂, AlCl₃)

Leaching conditions: 12M HCl, 75 °C, 3h



 $\rm H_2O_2$ concentration in leaching solution / vol%









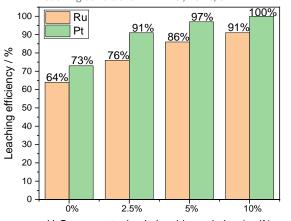
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H₂O₂ content (1-5%, 7.5%, **10%**, 20%)

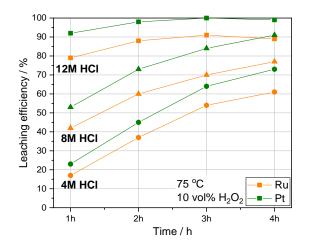
HCl concentration (2M, 3M, 4M, 8M, 12M)

Additives (NaCl, CuCl₂, AlCl₃)





H₂O₂ concentration in leaching solution / vol%

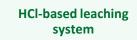










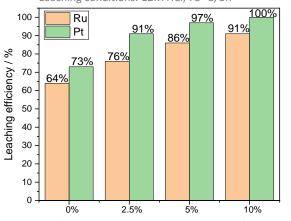


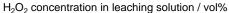
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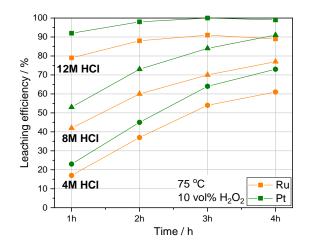
HCl concentration (2M, 3M, 4M, 8M, 12M)

Additives (NaCl, CuCl₂, **AlCl₃**)









AICI ₃	CuCl ₂	NaCl	Total Cl ⁻	Ru, %	Pt, %
0.5M	-	-	5.2M	72	81
-	0.75M	-	5.2M	56	67
-	-	1.5M	5.2M	73	82
-	1.5M	-	6.7M	79	90
1.5M	-	-	8.1M	84	96

Leaching conditions: 4M HCl, 75 °C, 5 vol% H₂O₂

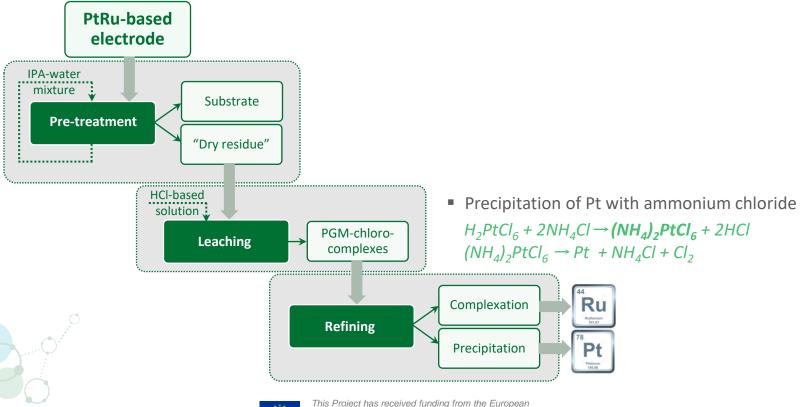






Recycling strategy





Union's Horizon 2020 Research and Innovation Programme under Grant Agreement N. 861960



- Effective **separation of the catalytic layer** by treating the electrode with isopropanol-water mixture.
- The influence of reagents concentration to optimize the leaching system was investigated.
- The use of chlorides lowers the required HCl concentration and the acidity of the leaching solution.
- Selective precipitation of Pt with the efficiency above 90 %.
- Recycling scheme for PGM recovery from spent electrodes has been proposed.



- Test multimetallic catalysts (e.g. Pt/Ru/Ir).
- Further investigation of the PGM separation from the leach solution.
- Reuse of obtained PGM complexes to manufacture the electrocatalyst.

Thank you for your attention! Questions?



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