

Kinetic Testing

- Test benches
- Loop Reactor
- NH₃-TPD, HTPD
- FTIR Spectrometers
- Mass Spectrometers
- GC/FID/MS
- Infrared Camera
- Soot Generator

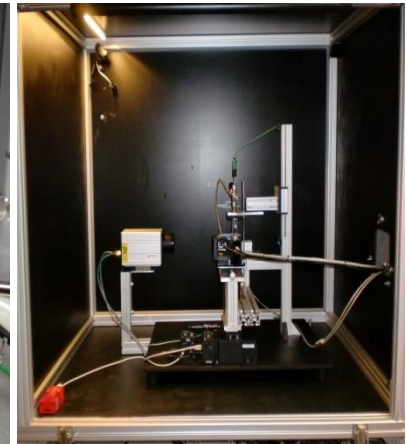
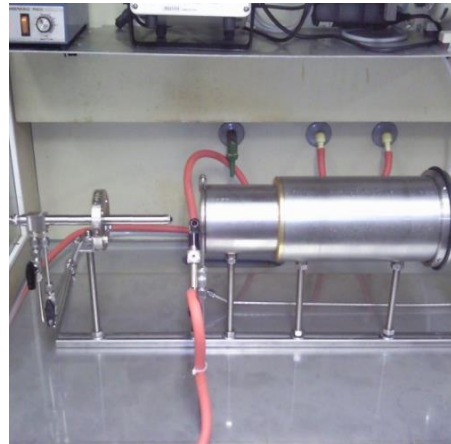


Characterisation

- DRIFTS, FTIR, ATR-IR
- UV-Vis
- Raman with Microscope
- ⁵⁷Fe Moessbauer
- XPS, XRD, XRF
- SEM
- ICP-OES
- Hg Porosimetry, BET

Preparation

- Flame Spray Pyrolysis
- Hydrothermal Synthesis
- Microwave
- Precipitation
- Complexation
- Ceramic Method

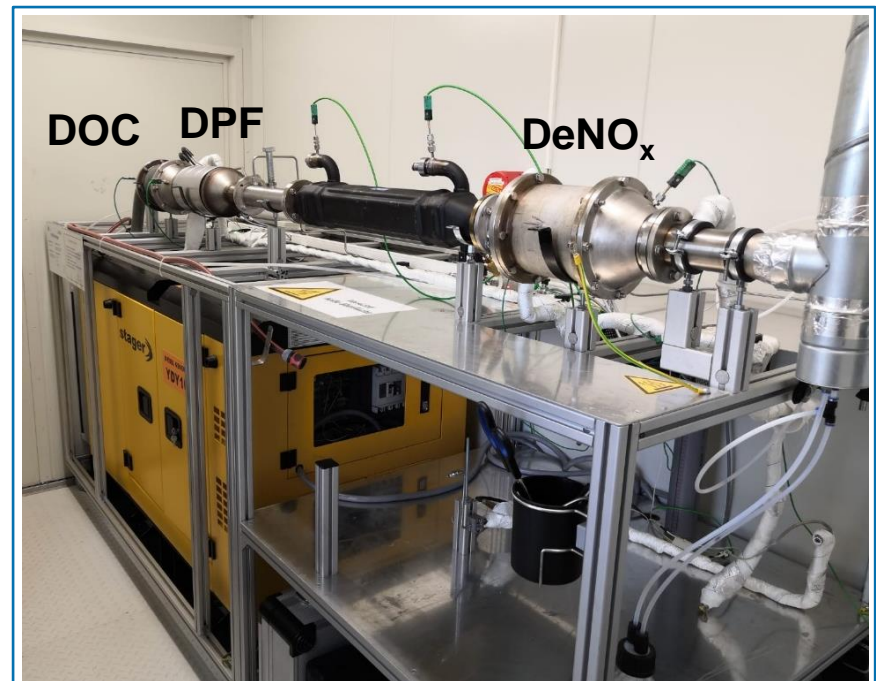


- DI diesel engine (emergency unit)
 - 11 kW at 1500 1/min
 - 3 cylinders, 1532 ccm
 - Compression ratio: 18:1
 - $\lambda = 2...5$

- Exhaust volume flow:
600...1000 l/min

- Exhaust mass flow:
40...60 kg/h

- Test of real catalysts:
DOC, SCR, H₂-deNO_x,
soot oxidation

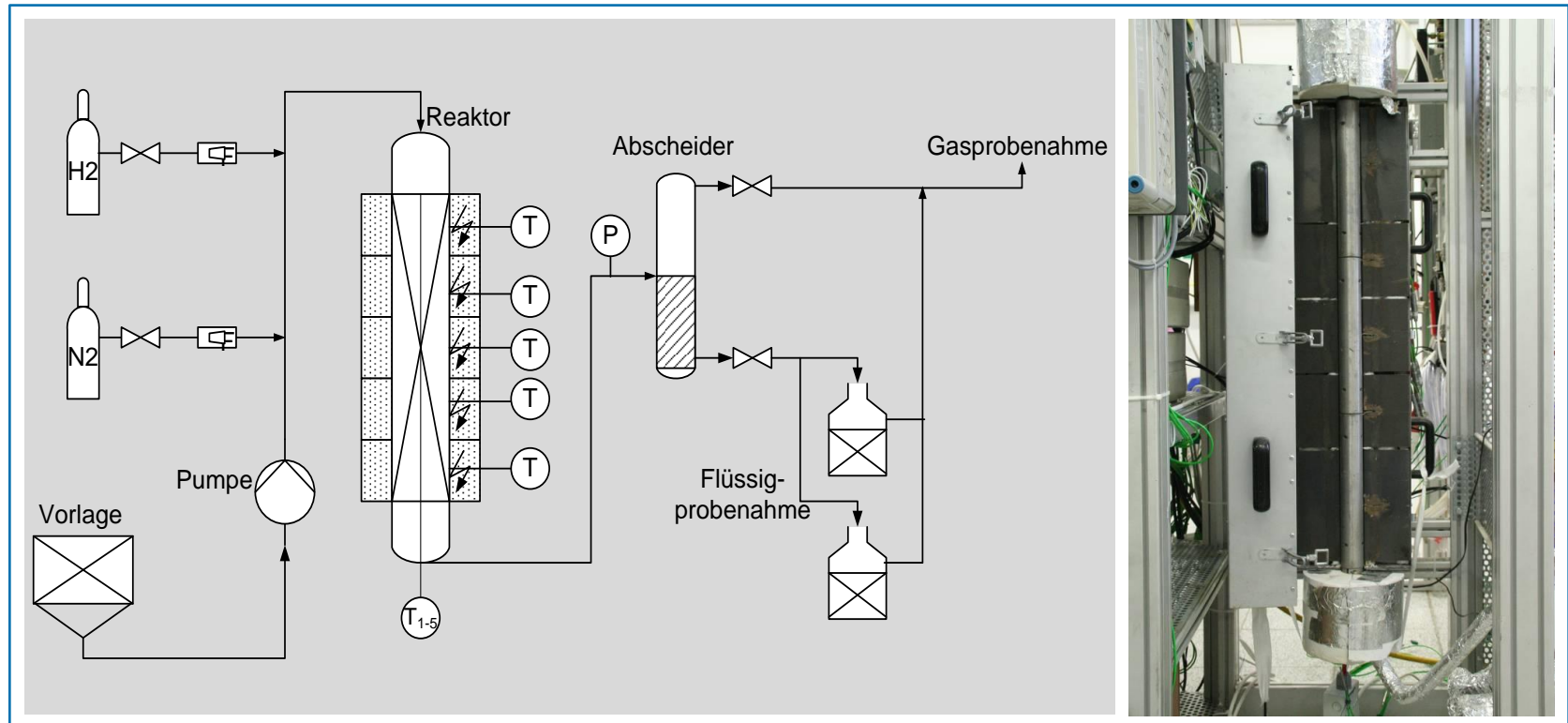


- Raw gasoline < 1 L/d
- Catalyst: $m < 60 \text{ g}$ (120 ml)
- SiC dilution of catalyst
- Isothermal fixed-bed reactor
- $T < 750^\circ\text{C}$, $p < 14 \text{ bar}$
- Periphery:
 - Pre-reactor for DME ($\gamma\text{-Al}_2\text{O}_3$)
 - Product separation at 5°C and ambient pressure
 - Continuous monitoring of gas flow
 - Oxidation catalyst for off-gas after-treatment



Operation Conditions:

- Catalyst Volume: ca. 100 ml
- Pressure: max. 150 bar
- Temperature: max. 400 °C
- LHSV: max. 4 h⁻¹
- Liquid Flow: max. 400 ml/h
- H₂ Flow: max. 300 l/h



- R&D using Fe catalysts
- Isothermal fixed-bed reactor
- Automatisierter Betrieb (SPS)
- Specification:
T < 500°C, p < 250 bar
- Total flow: max. 1000 ml/min
- Analytics:
Online NDIR spectroscopy for NH₃

